

EXPERIMENTAL DETAILS FOR LIGHT WATER COLD FUSION RESEARCH AT CAL. POLY.- POMONA

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ABSTRACT

This paper presents a detailed description of the construction and operation of the two types of electrolytic cells employed in the experimental light water cold fusion research of R. Bush and R. Eagleton at California State Polytechnic University - Pomona.

INTRODUCTION

Electrolytic cells of the Fleischmann and Pons^[1] type using light water with nickel cathodes and alkali carbonates were first employed at Cal. Poly - Pomona in August of 1991 following the announcement of excess heat production in light water by Mills and Kneizys^[2]. Cell design and protocol was partially driven by considerations based upon the theoretical work of R. Bush^[3]. Since that time a total of 27 light water cells have been run with alkali carbonate and alkali hydroxide electrolytes using two different cell and calorimeter configurations. These configurations and other details are described in this paper. The experimental results obtained with these cells are not discussed in this paper but are presented elsewhere^[4,5,6,7,8].

CELL AND CALORIMETER DESIGN

The two types of cells used in our light water work are actually third and fourth generation cell designs which evolved from earlier work with heavy water. Consequently these cell types are designated as C and D respectively. They are illustrated in figures 1 and 2. Cells of type C were first used with heavy water in July of 1990 and continued to be used until January 1993. During that period 17 light water cells and 36 heavy water cells were run. Type D cells were phased in commencing February of 1993 and used for all cells constructed from that time until the present. To date ten light water cells have been operated using the type D configuration. Table I gives a summary of the light water cells that have been run to date.

The principal features which are common to both cell designs are as follows:

(1) They are all closed cells. This is achieved by use of a platinum black recombiner which is enclosed in the air space above the electrolyte. The recombiner is fabricated by bonding platinum black to a nickel screen mesh and coating one side of the mesh with a non-wetting agent (Teflon). The recombiner for all cells of type D and some of type C were enclosed within a nickel foil baffle that had extensions on either sides which served to return the recombination heat back into the electrolyte. This baffle also served to protect the recombiner from becoming contaminated with electrolyte residue. The recombiner for type C cells that was not placed in the baffle arrangement was instead affixed to the bottom side of the stopper and was unshielded. The cell is vented to the atmosphere via an oil bubbler which serves two purposes: (a) to maintain near ambient pressures, and (b) to isolate the cell from the external environment. A

balloon attached to the open end of the bubbler is used to monitor a cell for recombiner malfunctions. Of the light water cells run to date no recombiner malfunctions have been experienced. (2) Magnetic stirring is used to permit more uniform electrolyte temperatures. Tests have shown that these stirrers have no measurable effect on the electrolyte temperatures. (3) All surfaces except for electrodes and the nickel heat sinks are coated with Teflon. The neoprene stoppers are covered with form fitting Teflon tape and the cells were either pyrex coated with Teflon (type C) or made of Teflon bottles (type D). A special bonding agent is required to prevent the Teflon from becoming unbonded from the pyrex upon repeated thermal cycling. It is anticipated that the nickel heat sinks exposed to the electrolyte should pose no problems since they are shielded electrolytically by the nickel cathodes. (4) The electrodes are as follows: Platinum (AESAR 99.95%) wire anodes were 1 mm diameter and lengths of about 18 cm folded into five equal segments, nickel fibrex cathodes were formed into open ended cylinders having the platinum anode located along their central axis. Figures 3 and 4 are electron micrographs of a typical piece of 80/20 nickel fibrex mesh. Shown in these micrographs are nickel powder (20%) bonded to nickel fibers (80%) where the fibers are about 20 microns in diameter (Fig. 4). Also it should be noted that the nickel fibers are not fabricated from drawn nickel wires but are made from sintered nickel powder. These fibers are formed by extruding a slurry of nickel powder mixed in a plasticizer through a small orifice. After the plasticizer sets, the fibers are sintered in a hydrogen environment so that only porous nickel remains after the heat treatment. (5) Electrolytes were made of chemicals obtained from AESAR/Johnson Matthey and nanopure water (17 Mohm-cm) from a Barnstead filtering system. All electrolytes were 0.57 molar solutions. (6) A port for extracting electrolyte samples consists of a capped 1 mm diameter Teflon tube which passes through the neoprene stopper and into the electrolyte. (7) The electrolyte temperature is monitored by use of two 26 gauge type-K thermocouples. These are threaded into opposite ends of a 1 mm diameter Teflon tube that loops through the neoprene stopper to just below the cathode and above the magnetic stirrer. This tube is filled with mineral oil to permit more efficient thermal contact of thermocouples with the electrolyte. As shown in figures 1 and 2 these thermocouples are placed at different depths in the electrolyte. We find that these thermocouples read very nearly the same temperature provided the magnetic stirrer is operative. However, in the event of a stirrer malfunction the thermocouple readings may differ by as much as two or three degrees Celsius.

Features that differ for the two cells types are as follows:

Cell Type C - As illustrated in Figure 1, this is a double wall pyrex vessel which provides for a water jacket enclosing the electrolytic cell except for the top which is capped with a Teflon covered neoprene stopper. The inlet and outlet coolant temperatures were monitored with type K thermocouples. The pyrex cell was completely enclosed with a one inch thick layer of styrofoam.

Calibration for these cells was performed in one of two ways: (1) Either a nichrome reference heater was used or (2) the cell was calibrated by running anodically. When a nichrome reference heater was used it was placed in a close fitting Teflon tube that looped down into the electrolyte. The nichrome heating element was attached to electrical leads so as to have it completely immersed within the electrolyte. The cell calibration procedure is as follows: (1) The temperature of the coolant flowing through the water jacket was regulated so as to maintain the cell contents at a constant temperature. A typical value for the cell operation temperature was about 39°C. At this temperature the cells could be calibrated from 0 to 20 watts while using the laboratory as the heat sink for the cell bath. Table II gives typical calibration data for this type of cell. Note that the standard deviation in the calibration temperatures is less than 0.1°C. The cell calibration data points are obtained by plotting the steady state thermal power output (P_{out}) from the cell as a function of the average temperature decrease (∂T) across the cell walls. This temperature decrease is found by taking the difference between the average of the two cell thermocouples

readings and the average of the inlet and outlet thermocouple readings. (For steady state calibration conditions the electrical power input to the cell is equal to the thermal power output.) This plot of P_{out} versus ∂T was fit by either a linear or a third order polynomial. Figure 5 shows a typical calibration curve that was obtained for cell 62. The excess power (P_{ex}) was determined by subtracting the electrical power delivered to the cell from the steady state thermal power coming out of the cell as calculated from the fit that yielded the smallest value for P_{ex} .

Cell Type D - Cells of this type are illustrated in Figure 2. They are constructed from Teflon bottles and are designed to be immersed directly within the coolant water bath. The bath water was temperature regulated as well as stirred. The calibration procedure for these cells are essentially the same as that for type C cells with the exception that the temperature decrease across the cell walls were obtained by subtracting the bath temperature from the average of the two cell thermocouple readings. Table III gives a typical set of calibration data for this type of cell.

Data Acquisition System

All temperatures, currents, and voltages were monitored and logged using a Macintosh IIX computer equipped with National Instrument's LabView software. For type C cells four type K thermocouples were used: one at the bath inlet port, one at the bath outlet port, and two within the electrolyte. In the case of type D cells there was one type K thermocouple within the bath and two within the electrolyte. The thermocouple sampling rate is 1000/minute with the temperature averaged each minute. The thermocouple voltages were converted to temperature readings ($^{\circ}\text{C}$) by use of AD595AQ/9217 integrated circuit chips. This system permitted steady state temperature measurements with standard deviations of about 0.05°C . Corrections for thermocouple temperature offsets were made within the software. Cell currents and voltages were logged from Fluke 45 dual display multimeters equipped with IEEE interface. Figure 6 shows a front panel view of the virtual instrument used for cell monitoring and control of data logging. Since our cells are calibrated for only steady state operation at a specified temperature, we make use of this virtual strip chart recorder to determine when the requisite conditions are achieved before logging data. Table IV gives a typical spread sheet of data logged for a cell which produced excess heat. Not shown but recorded with this spread sheet were the following: room temperature, multiplexer reference junction temperature, time mark and date mark. The data acquisition rate for both Table IV and Figure 5 was for one minute intervals. In Table IV it should be noted that the fractional uncertainty in P_{ex} about 2% for the 23 minute time interval shown there. However, all values of P_{ex} which we report are corrected for any differences found after recalibration.

ACKNOWLEDGMENTS

The following institutions are to be acknowledged for their support that has made this research possible: Southern California Edison, ENECO (Formerly FEAT of Salt Lake City, Utah). Roger Bush, son of R. Bush, is thanked for the software design of the virtual instrumentation employed in the data acquisition system.

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Cell #	Cathode	Electrolyte	Cell Type
38	Ni Fibrex	0.57M K_2CO_3 in 50cc H_2O	C
41	Ni Fibrex	0.57M K_2CO_3 in 50cc H_2O	C
44	Ni Fibrex	0.57M K_2CO_3 in 50cc H_2O	C
45	Ni Fibrex	0.57M K_2CO_3 in 50cc H_2O	C
47	Ni Fibrex	0.57M K_2CO_3 in 50cc H_2O	C
48	Ni Fibrex	0.57M Na_2CO_3 in 50cc H_2O	C
49	Ni Fibrex	0.57M Rb_2CO_3 in 50cc H_2O	C
50	Ni Fibrex	0.57M Rb_2CO_3 in 50cc H_2O	C
51	Ni Fibrex	0.57M Na_2CO_3 in 50cc H_2O	C
52	Ni Fibrex	0.57M Na_2CO_3 in 50cc H_2O	C
53	Ni Fibrex	0.57M Rb_2CO_3 in 50cc H_2O	C
54	Ni Fibrex	0.57M $RbOH$ in 50cc H_2O	C
55	Ni Fibrex	0.57M Rb_2CO_3 in 50cc H_2O	C
56	Ni Fibrex	0.57M $RbOH$ in 45cc H_2O +2cc D_2O	C
57	Ni Fibrex	0.57M Rb_2CO_3 in 50cc H_2O	C
61	Ni Fibrex	0.57M K_2CO_3 in 200cc H_2O	C
62	Ni Fibrex	0.57M $LiOH$ in 50cc H_2O	C
63	Ni Fibrex	0.57M K_2CO_3 in 62cc H_2O	D
64	Ni Fibrex	0.57M K_2CO_3 in 62cc dedeuterated H_2O	D
65	99.9975 Ni wire	0.57M K_2CO_3 in 60cc H_2O	D
66	99.9975 Ni wire	0.57M K_2CO_3 in 60cc H_2O	D
67	Ni Fibrex	0.57M K_2CO_3 in 70cc H_2O	D
68	Ni Fibrex+10%Cu	0.57M K_2CO_3 in 70cc H_2O	D
69	Ni Fibrex	0.57M Rb_2CO_3 in 65cc H_2O	D
70	Ni Fibrex	0.57M Cs_2CO_3 in 65cc H_2O	D
71	Ni Fibrex+10%Cu	0.57M Rb_2CO_3 in 65cc H_2O	D
72	Ni Fibrex+10%Cu	0.57M Cs_2CO_3 in 65cc H_2O	D

Table I: Details of Cell Type, Cathodes, and Electrolytes for all Light Water Cells Run as of 2/94.

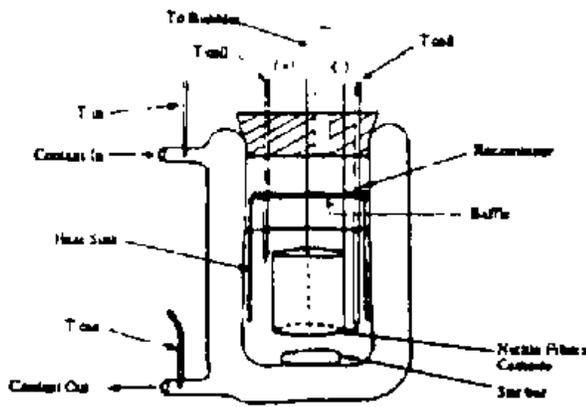


FIGURE 1. Third generation cell design: Cell type "C".

PRINCIPAL FEATURES

- CLOSED CELL OPERATION
- MECHANICALLY STIRRED ELECTROLYTE
- RECOMBINER Baffle & HEAT SINK
- TEFLON COATED PYREX CELL
- PLATINUM ANODE
- NICKEL FIBREX CATHODE
- NANOPURE H₂O BASE ELECTROLYTE
- CONSTANT COOLANT FLOW RATE
- CONSTANT CURRENT AND TEMPERATURE OPERATION

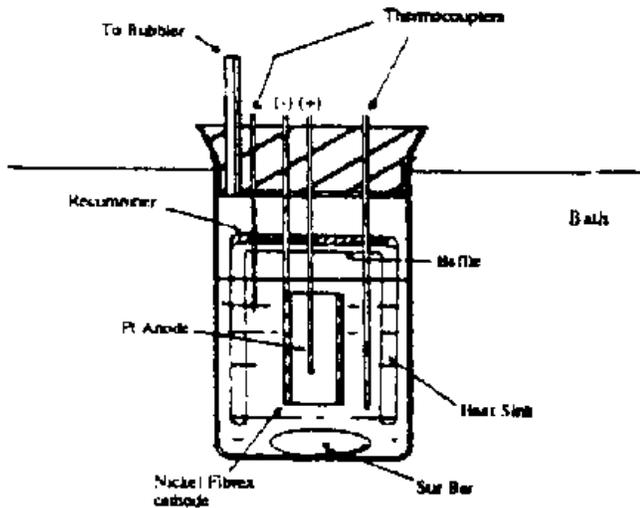


FIGURE 2. Fourth generation cell design: Cell type "D".

PRINCIPAL FEATURES

- CLOSED CELL OPERATION
- MECHANICALLY STIRRED ELECTROLYTE
- RECOMBINER Baffle & HEAT SINK
- TEFLON CELL
- PLATINUM ANODE
- NICKEL FIBREX CATHODE
- NANOPURE H₂O BASE ELECTROLYTE
- CELL IMMERSED IN BATH
- CONSTANT CURRENT AND TEMPERATURE OPERATION

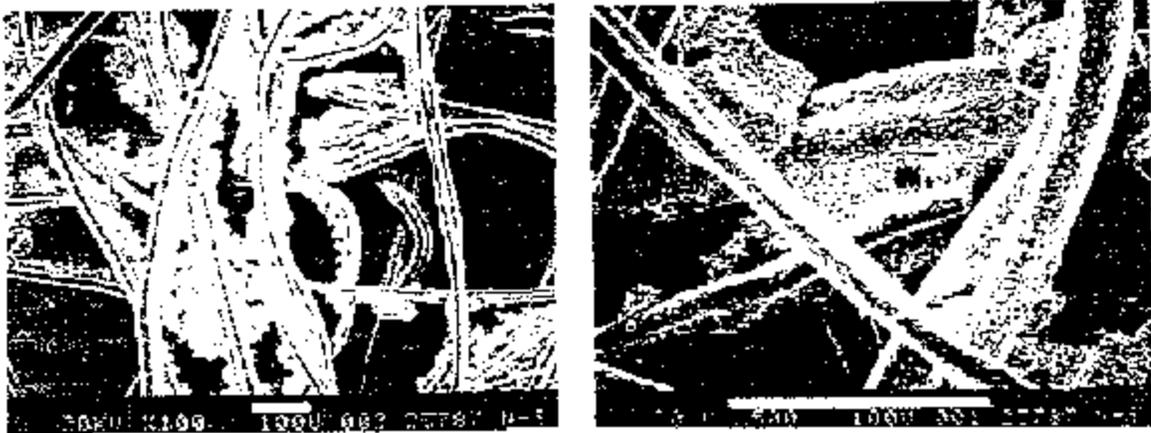


Figure 3. SEM photomicrographs of nickel fiber cathode material having 80% nickel fiber and 20% nickel powder for magnification of 100x and 500x.

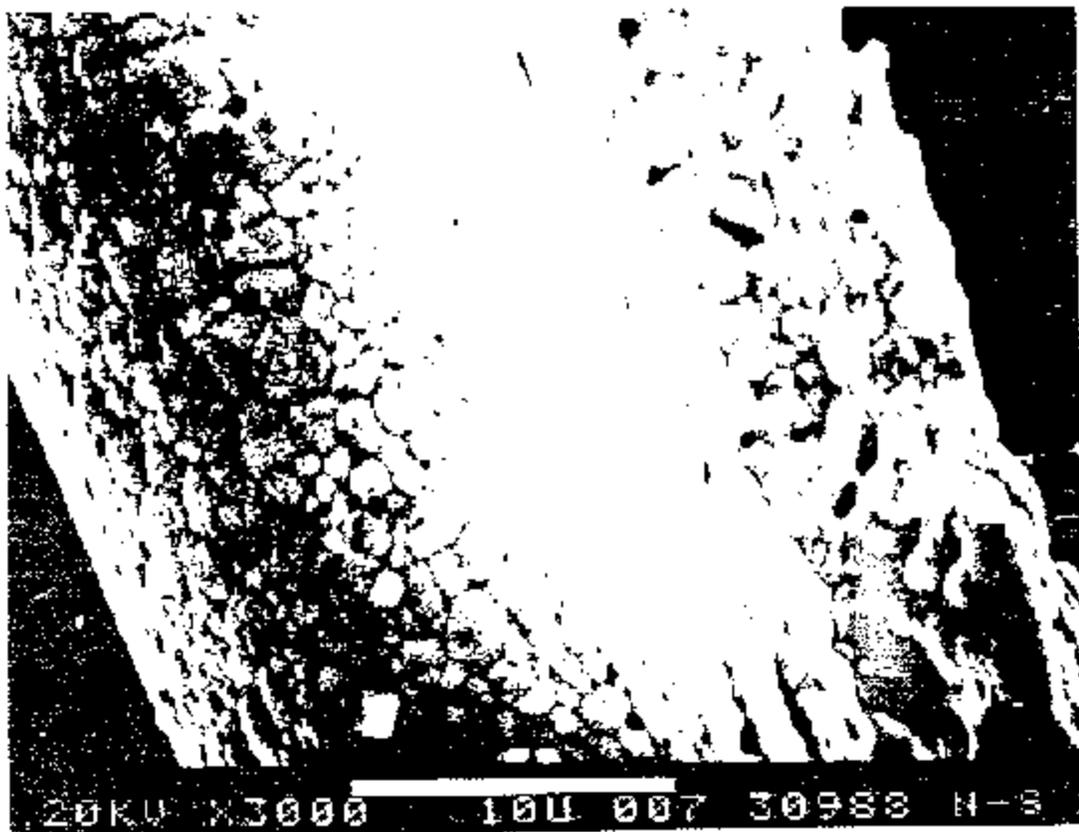


Figure 4. SEM photomicrograph of a single nickel fiber with a magnification of 3000x displaying its granular structure.

T _{cell}	T _{LD}	T _{conv}	T _{cell}	T _{LD}	T _{conv}	P _{in}	P _{out}	η _{cell}	η _{LD}	Time	Meas.
39.023	39.011	39.011	39.449	31.237	31.343	7.174	9.740	1.357	14.678	1:18:23	PM
39.023	39.043	39.034	39.469	31.209	31.329	7.225	9.721	1.336	14.643	1:18:24	PM
39.062	39.065	39.063	39.585	31.197	31.291	7.172	9.710	1.337	14.663	1:18:36	PM
39.130	39.067	39.049	39.472	31.144	31.283	7.265	9.726	1.327	14.655	1:18:54	PM
39.112	39.097	39.081	39.484	31.265	31.354	7.155	9.677	1.337	14.703	1:19:03	PM
39.087	39.095	39.076	39.474	31.115	31.295	7.175	9.761	1.337	14.710	1:19:24	PM
39.064	39.097	39.096	39.432	31.122	31.277	7.211	9.716	1.327	14.675	1:19:39	PM
39.085	39.040	39.072	39.442	31.119	31.310	7.189	9.751	1.329	14.619	1:19:54	PM
39.060	39.069	39.011	39.371	31.201	31.266	7.225	9.719	1.327	14.647	1:20:10	PM
39.117	39.049	39.040	39.417	31.172	31.290	7.249	9.675	1.328	14.571	1:21:46	PM
39.078	39.005	39.091	39.405	31.228	31.316	7.175	9.700	1.326	14.609	1:21:58	PM
39.121	39.039	39.020	39.424	31.183	31.334	7.225	9.715	1.328	14.631	1:22:11	PM
39.158	39.075	39.058	39.390	31.183	31.288	7.280	9.672	1.327	14.575	1:22:26	PM
39.129	39.020	39.024	39.439	31.189	31.312	7.212	9.746	1.328	14.683	1:22:41	PM
39.141	39.058	39.056	39.391	31.178	31.257	7.263	9.647	1.327	14.533	1:22:57	PM
39.097	39.093	39.045	39.433	31.188	31.339	7.234	9.674	1.328	14.589	1:23:12	PM
39.073	39.050	39.040	39.443	31.187	31.316	7.147	9.712	1.328	14.623	1:23:27	PM
39.123	39.028	39.070	39.429	31.150	31.299	7.287	9.598	1.328	14.407	1:23:42	PM
39.121	39.040	39.022	39.474	31.191	31.333	7.183	9.705	1.327	14.622	1:23:57	PM
39.121	39.012	39.059	39.444	31.213	31.328	7.241	9.745	1.328	14.673	1:24:12	PM
39.087	39.084	39.075	39.430	31.208	31.317	7.158	9.722	1.328	14.641	1:24:27	PM
39.081	39.024	39.028	39.414	31.214	31.314	7.214	9.710	1.327	14.633	1:24:42	PM
39.057	39.041	39.039	39.417	31.183	31.300	7.189	9.710	1.327	14.633	Averages	
0.088	0.065	0.049	0.024	0.026	0.018	1.047	0.002	0.000	0.042	S.d. Dev.	

Table II: Calibration data for $P_{in} = 14.6$ watts for cell 62 at $T_{cell} = 39C$.

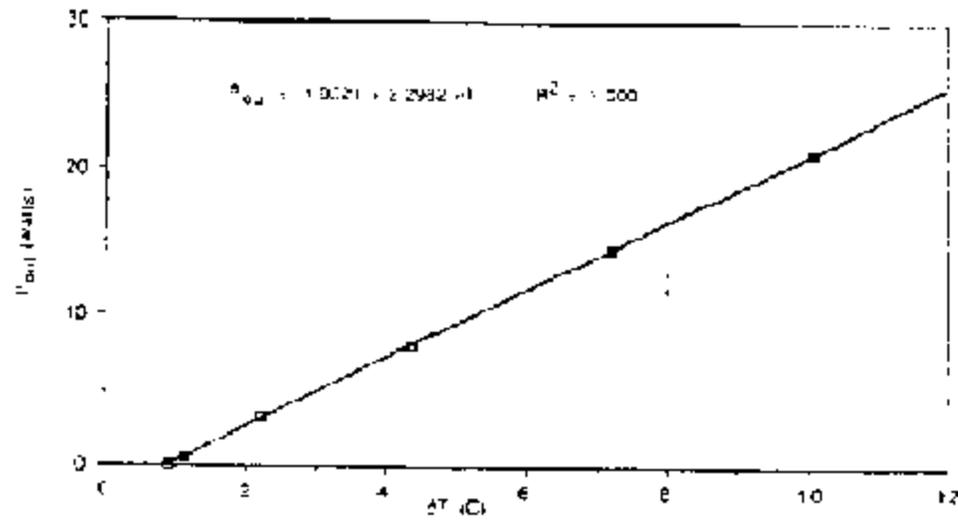


Figure 5. Calibration curve for cell 62 at a cell temperature of 39C

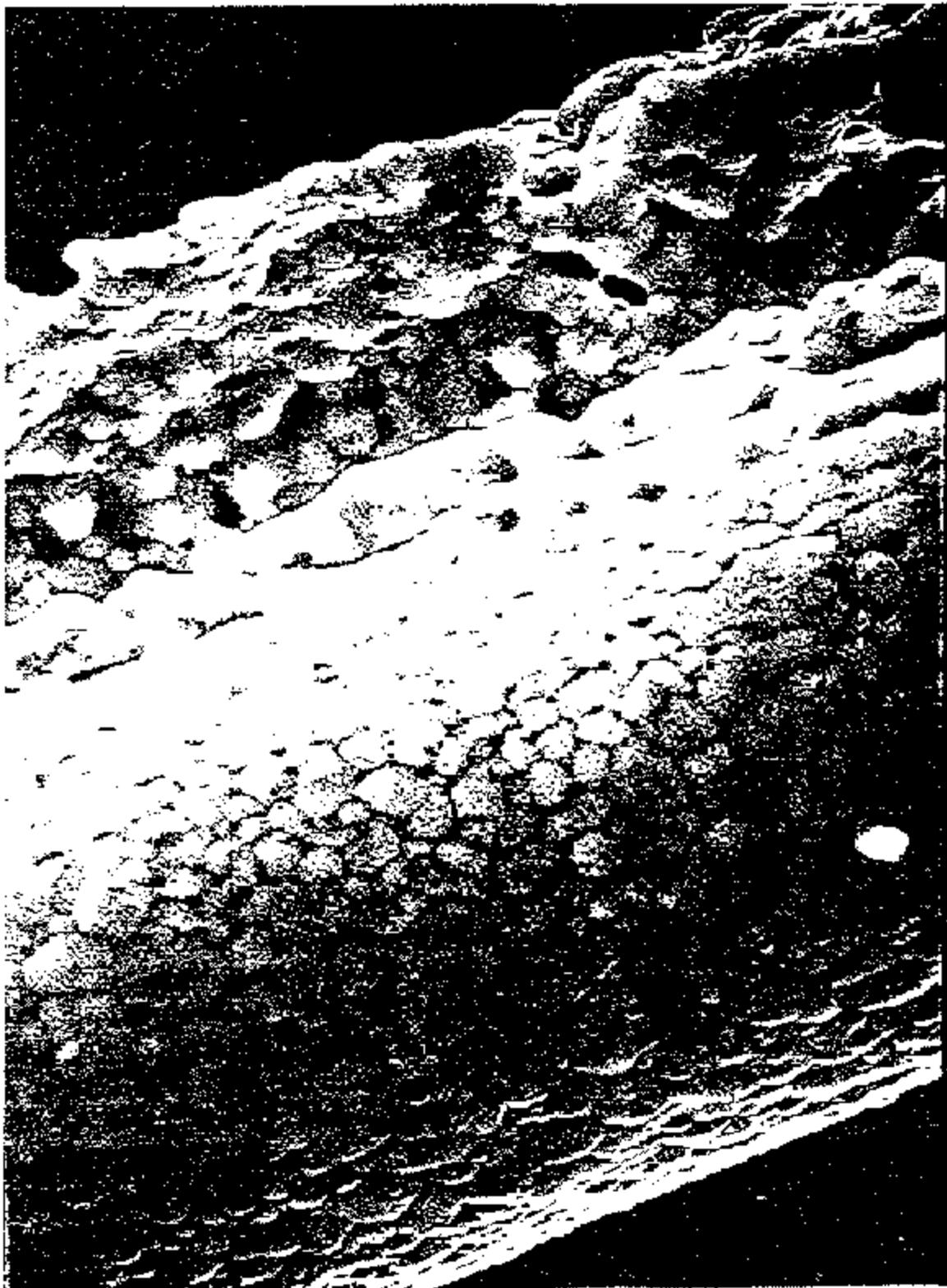
Tca	Tcd	Tavg	TDH2O	ai	IEff	VEff	Pineff	Pout	Rel
38 652	38 770	38 711	32 829	5 886	-2 100	-4 559	9 574		
38 689	38 761	38 725	32 852	5 872	-2 100	-4 585	9 628		
38 658	38 755	38 707	32 842	5 864	-2 100	-4 594	9 647		
38 648	38 761	38 705	32 850	5 874	-2 100	-4 556	9 588		
38 751	38 792	38 777	32 813	5 964	-2 100	-4 571	9 599		
38 761	38 792	38 777	32 813	5 964	-2 100	-4 571	9 599		
38 735	38 752	38 744	32 810	5 933	-2 100	-4 571	9 599		
38 658	38 749	38 709	32 805	5 903	-2 100	-4 580	9 618		
38 810	38 824	38 817	32 827	5 990	-2 100	-4 557	9 570		
38 729	38 772	38 751	32 853	5 896	-2 100	-4 564	9 584		
38 709	38 787	38 748	32 841	5 907	-2 100	-4 573	9 603		
38 750	38 806	38 793	32 830	5 963	-2 100	-4 564	9 584		
38 747	38 785	38 766	32 822	5 944	-2 100	-4 574	9 605		
38 747	38 785	38 766	32 822	5 944	-2 100	-4 571	9 599		
38 745	38 776	38 761	32 819	5 941	-2 100	-4 564	9 594		
38 841	38 826	38 834	32 803	6 030	-2 100	-4 560	9 576		
38 751	38 795	38 773	32 817	5 956	-2 100	-4 567	9 591		
38 731	38 782	38 756	32 825	5 931	-2 100	-4 569	9 596	Averages	
0 055	0 023	0 038	0 015	0 046	0 000	0 010	0 021	Std Dev	

Table III: Calibration data for $P_{in} = 9.59$ watts for cell 70 at 39C.

Tca	Tcd	Tavg	TDH2O	ai	IEff	VEff	Pineff	Pout	Rel
38 962	39 053	39 008	33 229	5 779	1 220	5 312	6 481	9 040	2 559
38 940	39 053	38 997	33 233	5 763	1 220	5 352	6 529	9 015	2 486
38 981	39 087	39 034	33 239	5 795	1 220	5 324	6 495	9 066	2 571
38 979	39 009	38 994	33 257	5 737	1 220	5 318	6 488	8 974	2 486
38 965	39 089	39 027	33 247	5 780	1 220	5 319	6 489	9 043	2 554
38 951	39 079	39 015	33 228	5 786	1 220	5 271	6 431	9 052	2 622
38 950	39 079	39 015	33 228	5 786	1 220	5 329	6 501	9 052	2 551
38 947	39 130	39 039	33 241	5 798	1 220	5 304	6 471	9 070	2 597
38 982	39 022	39 002	33 242	5 760	1 220	5 265	6 423	9 011	2 587
39 008	39 026	39 017	33 269	5 747	1 220	5 305	6 472	8 990	2 518
38 940	38 991	38 966	33 268	5 697	1 220	5 313	6 482	8 910	2 428
38 956	39 074	39 015	33 254	5 761	1 220	5 312	6 481	9 012	2 532
38 943	39 072	39 008	33 241	5 767	1 220	5 307	6 475	9 021	2 547
38 941	39 053	38 997	33 242	5 755	1 220	5 308	6 476	9 002	2 527
38 941	39 053	38 997	33 242	5 755	1 220	5 332	6 505	9 002	2 497
38 945	39 028	38 987	33 270	5 716	1 220	5 303	6 470	8 940	2 470
38 957	39 047	39 002	33 253	5 749	1 220	5 335	6 509	8 992	2 493
38 975	39 039	39 007	33 245	5 762	1 220	5 296	6 461	9 013	2 552
38 973	39 085	39 029	33 241	5 788	1 220	5 315	6 484	9 055	2 571
39 002	39 029	39 016	33 250	5 765	1 220	5 334	6 507	9 018	2 511
38 953	39 067	39 010	33 257	5 754	1 220	5 358	6 527	9 000	2 463
38 978	39 055	39 017	33 249	5 768	1 220	5 307	6 475	9 022	2 548
38 978	39 055	39 017	33 249	5 768	1 220	5 303	6 470	9 022	2 553
38 963	39 055	39 009	33 247	5 762	1 220	5 314	6 483	9 014	2 531
0 020	0 031	0 016	0 012	0 024	0 000	0 021	0 026	0 038	0 047

Averages
Std Dev

Table IV: Excess power data for cell 70 at 39C.



S-N 88603 200 001 0002X 0362

28KU W3000 100 007 30000 N-5

